



Performance enhancement of a Latent Heat Thermal Energy Storage for Domestic Hot Water production

B. Champel, A. Bruch, F. Bentivoglio

COMBIOTES Project



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Why Thermal Energy Storage for Domestic Hot Water Production?



Own calculations based on data from PVGIS, DHWcalc and RTE (French TSO)

- Peaks of Domestic Hot Water (DHW) consumption in the morning and in the evening
 - Simultaneous with peak of electricity demand
 - In opposite phase with solar profile

Thermal storage at residential scale

- Time-decoupling between heat production and consumption
- Combination with solar thermal
 Combination with heat pumps



Objective of the study

- Assessment of the performance in discharge of a Latent Heat Thermal Energy Storage for DHW production
- Investigation of design factors to enhance performance

Thermal Energy Storage (TES) to provide Domestic Hot Water (DHW) for a single-family house

• Requirements :

- Capacity : **9kWh** (Daily DHW need for 5-persons household ADEME, 2022)
- Draw off flow rate : 12 L/mn
- Draw off temperature : 40°C
- Water input temperature : 12°C
- **Charging phase** of the storage is not studied here (internal electrical charge assumed)
- Assumption that TES initial temperature is 75°C

Use Case

Storage Design





Schematic of a shell-and-tube Latent Heat TES (Bentivoglio et al, 2021, hal-03492919)

 (e_2)

- Based on **Shell-and-tube** Heat Exchanger concept
- Heat Transfer Fluid (HTF) = Water flows inside finned tubes
- Tube bundle (h) is surrounded by Phase Change Material (PCM) embedded in the shell (a)
- Inserts are placed inside the tubes (reduction of hydraulic diameter and thus Grashof number → forced convection flow regime)





System

Latent Heat TES outlet temperature decreases with time in discharge

Need to partly bypass TES in order to reach a constant temperature at the draw-off point

12 L/mn



Numerical Model

- Heat Transfer Fluid
 - assumed uniformly distributed over the tubes → 2 tubes modeled
 - 1D-axial discretization
 - Enthalpy and mass balance
 - Heat exchange coefficient calculated from classical correlations
- Insert, tube, fins and PCM
 - 1D radial discretization
 - Axial conduction neglected
 - Transient heat equation
 - PCM + fins : equivalent material properties

Model validated on experimental data

(Da Col et al, 2023, doi.org/10.1016/j.est.2023.109239)



Numerical Model



- **Useful capacity** = cumulative energy discharged until the moment when water temperature falls below the target temperature
- **Discharge efficiency** = ratio of useful capacity to energy stored between target and maximum temperature

Reference Design



47cm Design a mila 1 and Number of tubes 37 0) Single pass Tube network ۲ . arrangement PCM Octadecanol • (melting T° 58°C) 0 1.37m Tubes' height 1.37m Tube path network ۲ 67.2mm Shell diameter 0.47m 6) Average PCM height 1.27m 146kg PCM mass Energy stored betw. 16.2 kWh 40°C and 75°C

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Hydraulical tube

Heating tube

Heating cartridge

Insert

Reference Design



40°C and 75°C

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Number of tubes	37
Tube network	Single pass
arrangement	
PCM	Octadecanol
	(melting T° 58°C)
Tubes' height	1.37m
Tube path network	67.2mm
Shell diameter	0.47m
Average PCM height	1.27m
PCM mass	146kg
Energy stored betw.	16.2 kWh





Performance

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10

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Average PCM height	1.27m
PCM mass	146kg
Energy stored betw. 40°C and 75°C	16.2 kWh

Storage outlet T° Performance reaches target T° 80 Non-useful energy discharged 70 60 - Storage outlet temperature - Temperature after mixing bottom PCM temperature - medium PCM temperature top PCM temperature Discharged Energy 20

40

10

0

0

20

Useful capacity	8.9 kWh
Discharge efficiency	55%

60

Time [mn]

80

100

25

20

5

0

Impact of PCM

	1		
	Octadecanol	RT-70 HC	Stearic Acid
Melting temperature	58°C	70°C	70°C
Storage heat capacity (latent			
+ specific heat) in the range	372 kJ/kg	392 kJ/kg	320 kJ/kg
[12 – 75]°C		-	
Average density	789 kg/m ³	825 kg/m ³	892 kg/m ³
Storage density	81.5 kWh/m ³	90 kWh/m ³	79 kWh/m ³

• RT-70HC and Stearic Acid have higher melting temperatures than octadecanol

 Better storage heat capacity for RT-70 HC than for Stearic Acid

Impact of PCM

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 Better storage heat capacity for RT-70 HC than for Stearic Acid

PCM	Octadecanol	RT-70 HC	Stearic Acid
PCM Mass [kg]	146	152	165
Energy stored between 40°C	16.2	17.4	15.4
Useful capacity [kWh]	8.9	12.3 (+38%)	11.0 (+24%)
Discharge efficiency	55%	71%	71%

• Increase in Useful capacity if RT-70 HC or Stearic Acid is used

• Explaination

- Higher ∆T between PCM and HTF → improved heat exchange
- Higher melting T° → energy retrieved at higher T°

Impact of tube network arrangement



Impact of tube network arrangement



Tube network arrangement	Single pass	3-pass	37-pass
PCM Mass	146 kg (octadecanol)		
Energy stored betw. 40°C and 75°C	16.2 kWh		
Useful capacity	8.9 kWh	12.4 kWh (+39%)	16.5 kWh (+85%)
Discharge efficiency	55%	77%	102%

37-pass



- Increase in Useful capacity by re-arranging fluid flow inside tube network
- Explanation :
 - increased HTF velocity in the tubes → improved heat exchange

Optimal Design

Design

	Reference	Optimal
Tube network arrangement	Single pass	Three-pass
РСМ	Octadecanol	RT-70 HC
PCM mass	146kg	152kg
Energy stored betw. 40°C and	16.2 kWh	17.4 kWh





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Optimal Design

Design

	Reference	Optimal
Tube network	Single pass	Three-pass
PCM	Octadecanol	RT-70 HC
PCM mass	146kg	152kg
Energy stored betw. 40°C and 75°C	16.2 kWh	17.4 kWh
Useful Capacity	8.9 kWh	14.0 kWh
Discharge Efficiency	55%	80%



 Increase in Useful capacity and Discharge Efficiency for the Optimal Design



Conclusion

- In DHW applications, only the energy retrieved above a given temperature (depending on the user) is useful
 - → Only part of the stored energy is useful
- How can we increase **Useful Storage Capacity**?
 - 1. Increase the energy stored in the TES (by increasing PCM quantity or using a PCM with optimized thermophysical properties)
 - 2. Increase the share of stored energy that can be retrieved above a given temperature level
- Our study shows that it is possible to increase the Useful Storage Capacity by :
 - Choosing a PCM with a high melting temperature
 - Arranging the hydraulic circuit in the heat exchanger in several passes





Any question?

CEA-Liten, Grenoble, France

liten.cea.fr

benedicte.champel@cea.fr





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Numerical Model

• Insert, tube, fins and PCM : Transient heat equation

$$\rho \ Cp \ \frac{\partial T}{\partial t} = \frac{1}{r} \frac{\partial}{\partial r} \left(\lambda \ r \ \frac{\partial T}{\partial r} \right)$$

 $\rho, {\it Cp}, \lambda$: material properties defined as a function of T for each zone

- PCM : *Cp* integrates latent heat of fusion
- « PCM + fins » : equivalent material, properties calculated as a function of mass fraction, except for λ
- Heat Transfer Fluid : Mass balance + enthalpy balance

$$\frac{\partial(\rho V)}{\partial z} + \frac{\partial \rho}{\partial t} = 0$$

$$S\frac{\partial h}{\partial t} + \frac{\partial(\dot{m}Cp T)}{\partial z} = \alpha \ hp \ \Delta T_{HTF,wall}$$

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- α : heat exchange coefficient, calculated from classical correlations
- HTF is assumed to be uniformly distributed over the tubes
 - Model validated on experimental data (Da Col et al, 2023, doi.org/10.1016/j.est.2023.109239)

